**REVIEW PAPER** 



# A review on advanced physico-chemical and biological textile dye wastewater treatment techniques

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Abstract The utilization of dyes in textile industries has enormously increased in recent years and has created several environmental problems. Currently, several methods are in practice to treat wastewaters. Effective and efficient treatment techniques before the discharge of used water in the environment are the need of the hour. This short review covers the research and recent developments in advanced wastewater treatment techniques such as nanophotocatalysis, ceramic nanofiltration membranes, and biofilms. The primary intent of this review article is to contribute the ready-made references for the active researchers and scientists working in the field of wastewater treatment. This review has mainly focused on advanced physicochemical and biological techniques for the treatment of textile dye wastewaters. Further, the influence of various operating factors on the treatment, advantages, and disadvantages of various techniques was also discussed. The recently developed materials for wastewater treatment are also summarized based on the latest available literature.

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#### **Graphic abstract**



**Keywords** Wastewater treatment · Physicochemical · Biological treatment · Advanced oxidation processes · Membrane filtration · Nanocatalysts

#### 1 Introduction

Currently, contamination of water is one of the major problems of the entire globe, due to the improper discharge of used water of the industries into the environment, high utilization of chemical fertilizers in agricultural fields, construction of roads, buildings, etc. (Sharma and Bhattacharya 2017). Further, the population growth is very expeditious, which harms the availability of drinking water to everyone. Especially, industrialization and urbanization, pollution of water have accelerated on a large scale (Saha et al. 2017). There are many chemical industries which are dealing with the dyes and among them, the large quantity of dye utilization and wastewater discharge after the process is being done by the textile industries exclusively. In the process of fiber conversion to yarn, yarn to fabric, dyeing, and finishing the textile industries use a large volume of water, numerous chemicals, auxiliary chemicals, dyes, and sizing materials (Yaseen and Scholz 2019). The usage of such harmful materials has been resulting in water contamination and environmental pollution. The water released after the fabric preparation consists of dissolved solids, color, noxious metals (chromium), printing gums (pentachlorophenol, detergents), sequestering agents (trisodium polyphosphate and sodium hexametaphosphate, chlorine, azo dyes), and stain removers (CCl<sub>4</sub>, residual chlorine, fixing agents like; formaldehyde and benzidine). Most of the aforementioned chemicals are harmful and a threat to the environment (Hussein 2013; Ananthashankar and Ghaly 2013). Hence the wastewater is needed to be treated well before it is discharged into the environment or used for other purposes (Fallis 2007). For the dyeing process, 60-70% of azo group dyes are used by most of the textile industries and around 15-20% of the total dye is discharged into the environment during the process, which is dreadful harm to the environment (Akpan and Hameed 2009; Ouasif et al. 2013). To control such activities from the industries, the government of India through the Central Pollution Control Board (CPCB) has brought few regulations for wastewater discharge. According to the CPCB, the allowable limit of the textile dye wastewater discharge is reported as; total suspended solids (TSS): 100 mg/L, color: 5 mg/L, total dissolved solids (TDS): 2000 mg/L, chemical oxygen demand (COD): 250 mg/L, biochemical oxygen demand (BOD): 30 mg/L (Holkar et al. 2016). The majority of the dyes used in this process are mutagenic, toxic, and recalcitrant to the breakdown of the microbial action and also favors the formation of the carcinogenic integrated under anaerobic degradation (dos Santos et al. 2007). Furthermore, the high turbidity and the color discharged from the textile industries restrain the penetration of the oxygen and sunlight. These two sources are very much crucial for any living organism for their existence and this obstacle surely destroys the aquatic life (Crini 2006). The by-products of the dyes after degradation and the other related compounds present in the wastewater could damage human health and may lead to severe disorders such as Hemorrhage, mucous membranes, skin ulceration, and nausea (Solpan et al. 2003). This will also have a terrible and long-lasting impact on some of the important human body parts and systems like the liver, kidney, brain, reproductive system, and central nervous system (Kavipriya et al. 2002). Thus, to minimize the toxicity, pollution, and to protect the environment, it is important to treat the dye wastewater before discharge.

In this review, advanced treatment methods of wastewater such as nanophotocatalyst application, ceramic membrane filtration, nanophotocatalysis coupled with ceramic membrane filtration and wastewater treatment using chemical and biological methods including application of biofilms, are discussed in detail.

# 2 Advanced oxidation process for wastewater treatment

Both organic and inorganic pollutants present in the wastewater are removed by a set of chemical treatment methods. Among various chemical processes for used water, the oxidation process is broadly employed and known as the advanced oxidation process (AOP). In this process, for water purification, an adequate amount of hydroxyl radicals ( $OH^{\bullet}$ ) are generated and this notion was later expanded to sulfate radicals ( $SO_4^{\bullet-}$ ) oxidative processes. Apart from the degradation of organic and inorganic pollutants, AOPs are also been studied for the pathogen and pathogenic indicators inactivation. The recalcitrant organic pollutants

present in the wastewater can be swiftly degraded by the strong oxidants and hence AOPs have been considered as the best technologies for the wastewater treatment (Deng and Zhao 2015). Some of the recent studies on textile dye wastewater treatment using AOPs are discussed below in the Table 1.

Guimarães et al. (2012) studied the Reactive Blue 19 dye degradation by employing several AOPs such as the photo-Fenton process,  $H_2O_2/Fe^{2+}$ ,  $H_2O_2/UV$ , peroxidation, UV, etc. The schematic experimental setup was represented below (Fig. 1). At 500 mg/L  $H_2O_2$  and 3 h reaction time, 91% of dye was degraded by the  $H_2O_2/UV$  process. Within a very short span of the reaction, more than 98% of color and 36.8% of dissolved organic carbon were removed by the Fenton reagent. A reduction of 93, 80, 85, and 88% of BOD, COD, color, dissolved organic carbon respectively was observed when the photo-Fenton process was integrated with the biological system.

## **3** Nano photocatalyst application in wastewater treatment

The advanced oxidation processes (AOPs) have gained exceptional recognition concerning the advancement of wastewater treatment technologies for two decades. Some of the methods, including Fenton, cavitation, ozonation, and photocatalytic oxidation have been effectively utilized for the breakdown of recalcitrant organic contaminants at the pilot scale. Research has been done beforehand on both the homogenous and heterogeneous AOPs in the wastewater treatment domain. Catalysts such as TiO<sub>2</sub>, ZnO, UV/visible light, various oxidants such as H<sub>2</sub>O<sub>2</sub>, O<sub>3</sub>, etc. are employed to stimulate AOPs. At the time of activation, AOPs produce <sup>•</sup>OH radicals and react with organic composites in the proximity of dissolved O<sub>2</sub> of solvent media. Amid, several other industries, dyeing, printing, and paper industries are highly polluting the environment and this is because of the immense usage of the organic dyes in the course of the process. The absorption and reflection of the sunlight will be hindered because of the presence of organic dyestuffs in water bodies. Thus it results in an increase in noxious concentration which eventually troubles the aquatic life. Absolute mineralization of organic colorants can be achieved by employing dynamic AOPs. Several studies on different AOPs have

Method	Wastewater	Results	References
Heterogeneous Photocatalysis	Remazol Brilliant Blue R, Red Procion, Yellow Procion (EFA, EFB, and EFC textile industry effluents)	More than 90% of COD removal was achieved, and the $H_2O_2$ added was completely absorbed. At 430 nm, 100 and 67.36% of EFC and EFB effluents were degraded.	Garcia et al. (2007)
Chemical treatment techniques like Fe <sup>2+</sup> /H <sub>2</sub> O <sub>2</sub> , H <sub>2</sub> O <sub>2</sub> /UV, O <sub>3</sub> , etc. and advanced oxidation processes	Color and COD removal from acetate and polyester fiber dyeing effluent	AOP results in 60% of COD and 50% of color removal, while 96% of color and 99% of COD removal was achieved by integrating the AOP with the O <sub>3</sub> /H <sub>2</sub> O <sub>2</sub> /UV conventional method.	Azbar et al. (2004)
Advanced oxidation processes (AOPs)	Cotton-textile dyeing wastewater	At 60 mg catalyst loading, $85.5\%$ mineralization, and $98.5\%$ decolorization was achieved in the solar-photo-Fenton process. While, by integrating the biological process with solar-photo- Fenton reaction, $0.5$ kJUV/L of photo treatment energy and 7.5 mM of H <sub>2</sub> O <sub>2</sub> is required to attain the COD below 250 mg O <sub>2</sub> /L.	Soares et al. (2014)
Advanced oxidation processes (H <sub>2</sub> O <sub>2</sub> /UV, UV, O <sub>3</sub> )	Textile dye bath effluent	On the application of $H_2O_2/UV$ on biotreated dye bath effluent, 98% of decolorization was achieved. Application of AOPs following the biotreatment has surpassed the biodegradability.	Muhammad et al. (2008)

Table 1 Application of advanced oxidation processes (AOPs) for the treatment of various textile effluents containing dyes



**Fig. 1** System set-up for Reactive Blue 19 dye degradation by advanced oxidation processes, in which (1) a magnetic stirrer; (2) a reservoir of 9 L capacity; (3) a flow pump, and (4) a photoreactor (Reprinted from (Guimarães et al. 2012), Copyright (2012) with the permission from Elsevier)

explained the successful breakdown of the dye contaminants in aqueous media. The photocatalytic AOP could commence the intricate chain reactions and there is also a chance of generation of uncolored organic intermediates and the generated intermediates sometimes become poisonous. Many previous studies have revealed that for the breakdown of the organic composites, microsize catalysts were used in different AOPs, but utilization of nanomaterials in AOPs for the wastewater treatment has not been reported (Geng et al. 2009; Chang et al. 2009). Some of the semiconductors like TiO<sub>2</sub>, CdS, ZnO, WO<sub>3</sub> have been used as photocatalysts have been reported by Elamin and Elsanousi (2013). Among the photocatalytic materials, such as ZnO is considered one of the finest materials for the efficient breakdown of organic contaminants. Various studies have also revealed, that ZnO is highly photochemically reactive, economical and non-toxic and in terms of organic contaminants breakdown, as compared to TiO<sub>2</sub> (Pardeshi and Patil 2009; Strunk et al. 2009; Ali et al. 2010; Huang et al. 2012; Danwittayakul et al. 2013, 2015). It would be advantageous if ZnO assimilates visible light apart from UV light and it will benefit in the enhancement of

Method	Wastewater	Results	References
Photocatalysis/Mn-doped ZnO particles	Methylene Blue	The experiments were conducted separately with Mn-doped ZnO particles and undoped ZnO and observed that the doped particles have degraded the MB dye stuff more effectively and quickly than the undoped particles. $50\%$ of MB dye was decolorized in 5 min with ZnO:Mn <sup>2+</sup> and UV.	Ullah and Dutta (2008)
Photocatalysis/ZnO	Basic Blue 11 (BB 11)	It was observed that N- hydroxy alkylated byproducts were generated and BB 11 dye has undergone oxidative breakdown under UV irradiation, and <sup>•</sup> OH radical was major oxidant in this process. It was observed that in 24 min, 0.05 g/L of dye was degraded to 1% approximately $[1-(C/C_0)]$	Lu et al. (2009a)
Photocatalysis/Nd-doped TiO <sub>2</sub> films	RhodaminB	Photocatalytic action of the doped $TiO_2$ films was assessed under UV light by employing the textile industry contaminant Rhodamine B (RhB) and it was noticed that in 30 min of initial time 98% of RhB dye was removed.	WU et al. (2009)
Photocatalysis/ZnO/ZTO composites	Methyl Orange (MO)	By employing porous-ceramic-supported catalysts (CZnO/10ZTO) and under UV light irradiation 50% of MO dye was degraded in 1 h and approximately 95% of dye was degraded in 3 h. The photocatalytic activity was enhanced because of the ZTO islands, that were formed on the ZnO nanorods.	Danwittayakul et al. (2013)
Photocatalysis/ZnO/ZTO composites	Organic dyes	On irradiating the textile wastewater by sunlight, 77% of COD removal and 50% of photocatalytic breakdown efficiency was achieved by employing ZnO/15ZTO photocatalyst. The results were promising when the ZnO/15ZTO catalyst was used under solar light irradiation and about 16% degradation efficiency was increased. Figure 2 explains the SEM and EDS results of ZnO/ZTO composite oxides with different compositions synthesized on ZTO seeded substrate: (a) ZnO/5ZTO, (b) ZnO/10ZTO, (c) ZnO/15ZTO	Danwittayakul et al. (2015)
Photocatalysis/synthesized ZnO	Malachite green (MG)	The photodegradation of malachite green (MG) dye was studied by using ZnO photocatalysts synthesized by various techniques. And also, the impact of several operating conditions, including pH, catalyst loading, light source, and initial dye concentration on MG dye breakdown was analyzed. Under UV light, 93.75% of dye was degraded.	Saikia et al. (2015)
Heterogeneous photocatalysis/UV-C/TiO <sub>2</sub> (PET)/H <sub>2</sub> O <sub>2</sub>	Leaf green dye	The leaf green dye from the aqueous solution was removed by employing TiO <sub>2</sub> photocatalyst immobilized on polyethylene terephthalate (PET) plates and also in suspension form under UV light irradiation. 52% of TOC and 70% of COD reduction was achieved in UV-C/TiO <sub>2</sub> (PET)/H <sub>2</sub> O <sub>2</sub> system.	Aquino et al. (2019)

 Table 2
 Application of UV-visible induced nanomaterials as photocatalysts for the degradation of different organic contaminants in aqueous solutions

photocatalytic efficiency. Moreover, it is possible to absorb the visible light by bifurcating the ZnO bandgap into various sub gaps, and the bifurcation of ZnO can be attained by nitrogen doping (Elamin and Elsanousi 2013). Different researchers have reported, that since two decades the utilization of nanocrystalline ZnO and TiO<sub>2</sub> as photocatalysts for the breakdown of organic contaminants has been largely improved (Moon et al. 2003; Suárez-Parra et al. 2003; Yu et al. 2005; Peng et al. 2006b; Min et al. 2007; Venkatachalam et al. 2007; Wang et al. 2007; Pouretedal et al. 2009).

$$OH + h^+ \rightarrow OH$$
 (1)

$$H_2O + h^+ \rightarrow OH + H^+$$
 (2)

About 70–80% of the literature in the wastewater treatment using photocatalysis and  $ZnO/TiO_2$  as a photocatalyst is accessible and few researchers have



Fig. 2 SEM images and EDS results of ZnO/ZTO composite oxides with different compositions synthesized on ZTO seeded substrate: a ZnO/5ZTO, b ZnO/10ZTO, c ZnO/15ZTO

(Reprinted from (Danwittayakul et al. 2015), Copyright (2014) with the permission from Elsevier)

trialed the utilization of doped TiO<sub>2</sub> for the pollutant degradation. TiO<sub>2</sub> photocatalyst is called as semiconductor because it consists of a wide bandgap (3.2 eV) and parallel to radiation in the close UV range is beneficial compared to other photocatalysts. The ZnO/ TiO<sub>2</sub> particles get excited on UV light irradiation and produce a set of holes and electrons in the valence and conduction band. The charged species could relocate to the surface of the particle or they can combine with the dissolute heat from the absorbed energy and the holes to form hydroxyl radicals (OH·) reacts with OH<sup>-</sup> group and adsorbs H<sub>2</sub>O molecules.

To begin with the photocatalytic reaction wherein the organic contaminants breakdown in wastewater, both the light source and photocatalyst are mandatorily required. Recent studies have focused on the feasibility usage of visible light/sunlight for commencing the photocatalytic reaction and this will save a lot of energy, resources and also reduce the operating costs. Some of the recent studies on textile dye wastewater treatment using photocatalysis are discussed below in Table 2.

### 4 Ceramic membrane filtration in wastewater treatment

Recently, the ceramic membranes are gaining great attention, because of their superior characteristics like a long operating cycle, simple cleaning, regeneration, good chemical reliability, and pollution-free in the application of treatment of wastewater (Meabe et al. 2011). In the past, the ceramic membrane had limited application range, and was very expensive (Fujioka et al. 2014). But, later on, advancements in membrane research have resulted in the utilization of membrane technology for various purposes and have become cost-effective (Lee et al. 2015). Because of the fouling issue, the influent water standards are to be analyzed before the ceramic membrane is utilized in the industrial wastewater treatment process. In removing the pollutants from the wastewater the ceramic membrane follows two steps (Ali et al. 2017). All the particles that are enormous than the membrane size are blocked by the membrane, known as the selfretaining activity of the membrane. The smaller molecular weight particles will be absorbed by the membrane due to electrostatic forces, chemical bonds, and Vander Waals forces and this is known as the adsorption potential of the membrane (Zhao et al. 2018). Depending on the pore size, the membranes are

Table 3	Application of	ceramic m	nembrane :	filtration f	or the	treatment	of o	different	organic	contaminants	in aqu	ueous solution	
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Method	Wastewater	Results	References	
Integrated flocculation, cross- flow microfiltration, and ceramic membranes	Sulfur black, 2,3-acidic and DSD acidic wastewaters	The results have shown the decline of absorbency of sulfur black, DSD acidic, 2,3-acidic wastewater, and CODcr. At 0.1 MPa operating pressure and 1.0 µm ceramic membrane 93.3, 44.1 and 32.1% of absorbancy was achieved for sulfur black, 2,3-acidic wastewater, and DSD acidic wastewaters respectively.	Xu et al. (2002)	
Three materialistic ceramic membranes of different molecular weight cut-offs	Textile dye wastewater	The experimental results have shown, increase in permeate flux, a very little cake layer formation on the membrane, and minimal flux removal. Moreover, at the lowest cross-flow velocity, higher conductivity retention coefficients, and COD were acquired. The color and turbidity rejections were observed between 98% and 84% respectively.	Barredo- Damas et al. (2010)	
Integrated ceramic membrane and ultrafiltration	Textile wastewaters containing a reactive dye [Reactive Black 5 (RB5)] and NaCl	Under high pressure, very minimal color removal and maximum flux decline were observed from the experimental results. The solutions having exclusively RB5 were decolorized by more than 70% during filtration. On the addition of NaCl to the solution, minimal rejection of color and maximum decline of flux was also observed. The authors have mentioned that this could be due to the repulsion-attraction phenomena and membrane charge. It was also mentioned that the performance of the ultrafiltration and the membrane fouling effect was majorly influenced by the electrostatic interactions between the membrane materials and solute particles.	Alventosa- Delara et al. (2014)	
Ceramic microfiltration membrane (Manufactured with mineral coal fly ash)	Textile dye effluents	A significant decline in the color of 90% and 75% of COD was observed. The researchers have compared and contrasted the permeate flux performance with a commercial membrane and observed the similarity.	Jedidi et al. (2011)	

divided into four types namely; microfiltration, ultrafiltration, nanofiltration, and reverse osmosis (Jepsen et al. 2018). Excluding RO, the other three different membranes are employed in industrial wastewater treatment applications (Van Geluwe et al. 2011). Based on the shape, ceramic membranes could be classified into four types namely such as singlechannel tubular, multi-channel tubular, flat, and hollow fiber membrane (Wang et al. 2018). In the wastewater treatment process, the hollow fiber membrane is mostly employed. The flat membrane is widely used in the water resources area and the tubular membrane is employed in solid–liquid separation (Wang et al. 2018). Few recent studies on textile dye wastewater treatment using ceramic membranes are discussed below in Table 3.

Various investigators used ceramic membranes and revealed that they are alternative to polymer membranes and have extraordinary characteristics like physical, mechanical, lower cleaning frequency, thermal stability, longer lifetime, chemical resistance (Karnik et al. 2005; Dow et al. 2013; Muthukumaran and Baskaran 2014). Barredo-Damas et al. (2012) have treated textile mill effluents by tubular ceramic ultrafiltration membranes at various operating constraints like molecular weight cut-off, pH, and transmembrane pressure. Figure 3 is showing the schematic illustration of the wastewater treatment plant. The mixed waste streams are propelled into a



Fig. 3 Schematic illustration of the current wastewater treatment plant (Reprinted from (Barredo-Damas et al. 2012), Copyright (2012) with the permission from Elsevier)

dynamic rotating screen to remove bigger particles, then pH is regulated to 10.5 and sent to an equalization tank. Later, the solution is sent into a biological reactor, and to detach the activated sludge the effluent is driven into a dissolved air flotation tank (DAF). From the results, it has been observed that, for higher pressures, up to pseudo-stable values the permeate flux has been enhanced and 93% of turbidity, 96% of color, and 70% of COD removal have been observed from wastewater.

### 5 Nanophotocatalysis coupled with ceramic membrane filtration for wastewater treatment

The life span of the membrane decreases when the membrane undergoes fouling because of the precipitation or adsorption of molecules on its surface (Meng et al. 2009; Liu et al. 2010). The schematic illustration of the formation and removal of removable and irremovable fouling in MBRs was explained in Fig. 4. By applying physical cleaning, the removable fouling can be detached comfortably but chemical cleaning is required for irremovable fouling. Reversible fouling and removable fouling are similar. The reasons for the irremovable fouling and removable fouling are pore blocking and loosely attached foulants. This fouling complication is more conspicuous in ceramic and polymeric membranes. By

integrating the photocatalytic system with membrane separation the fouling problem could be surpassed (Zhang et al. 2006a; Pidou et al. 2009). In the integrated hybrid system, because of the photocatalysis process, the ceramic membrane dismisses the suspended photocatalysts as well as the degraded the organic contaminants.

The hybrid method could be used as an application in the treatment of several wastewaters, breakdown of various organic contaminants, and also removal of dyes like methyl orange, direct black, congo red, methylene blue, etc. from textile dye wastewaters (Naresh Yadav et al. 2018). Several researchers have worked on the integrated hybrid system and the design and working conditions of each study are different from the other. In some research works, the membrane was submerged in the photocatalytic reactor, and in other studies, both the systems were combined sequentially (Li et al. 2019; Donkadokula et al. 2020). Most of the researchers have utilized polymeric membranes for the combination with the photocatalytic process and very few researchers have used ceramic membranes in the integrated process (Song et al. 2018). Few recent studies on textile dye wastewater treatment using nanophotocatalysis coupled with ceramic membrane filtration are discussed below in Table 4.

The exotic materials like graphene oxide- $TiO_2$  (rGO/TiO<sub>2</sub>) and altered TiO<sub>2</sub> with an organic shell



**Fig. 4** Schematic illustration of the formation and removal of removable and irremovable fouling in MBRs (Reprinted from (Meng et al. 2009), Copyright (2009) with the permission from Elsevier)

layer was blended and fixed on the surface and pore structure of the monoliths (Athanasekou et al. 2013). They have studied the impact of various operating conditions including flow rate, feed concentration, and feed pressure on the membrane permeability and the efficiency of contaminants breakdown. Further, they have focused on the breakdown and removal of methyl orange (MO) and methylene blue (MB) under visible light irradiation and near-UV/Vis, and continuous flow photocatalytic filtration. From the results, it was observed that out of all the membranes, membrane N-TiO<sub>2</sub>-10 has exhibited excessive MB dye removal efficiency i.e. 57% under UV. Moreover, another research group investigated the photooxidation of organic pollutants present in the wastewater by using silica/titania nanotubes composite membranes. By utilizing porous alumina support membranes, the silica/titania membranes were formulated from silica/titania sols. The water contact angle has declined from 62° to nearly 5° in 80 min because of the surface membranes, which has shown an intense affinity for water under UV irradiation. For Direct Black 168 dye at 100 min of experimental operation, 73 and 66% of degradation were achieved in individual membrane separation and photocatalysis. Further, by integrating both the systems, i.e., the photocatalysis and the membrane separation process, 85% removal efficiency was achieved. From these results, it was concluded that the silica/titania nanotubes used in this study had multifunctions such as breakdown, refinement of membrane flux in photooxidation, and separation of organic pollutants in wastewater (Zhang et al. 2006b). Morover, Mozia (2010) explored the breakdown of toxic organic compounds in the presence of a photocatalytic membrane reactor using immobilized TiO<sub>2</sub> particles onto the surface of polymeric

Method	Wastewater	Results	References
Poly tetra fluoro ethylene (PTFE) membrane module submerged in TiO <sub>2</sub> slurry photocatalytic reactor	Reactive Black 5 (RB5)	At hydraulic retention time (HRT) of 4 h, 45–93% of TOC, 82–100% of color and 50–85% of COD was removed	Damodar et al. (2010)
Integrated microfiltration process with heterogeneous photocatalytic system	C.I. Disperse Red 73	60–90% of dye degradation and 98% of COD removal was achieved from the individual photocatalysis system	Buscio et al. (2015)
Integrated photocatalytic membrane reactor	Congo red dye	By utilizing PVP (ZnO-PVP-St) under stirring stipulations and in the absence of agglomerations four kinds of Zinc Oxides were fused. At 0.3 g/L ZnO-PVP-St loading $65 \pm 1.0\%$ and $100 \pm 0.5\%$ of dye degradation was observed after photocatalysis and nanofiltration respectively. The minimal membrane flux removal and higher photodegradation coherence in MPR were achieved due to the presence of ZnO-PVP-St	Hairom et al. (2014)
Combined ceramic membrane system with photocatalysis	Methyl Orange (MO)	The study has revealed that the integration of both systems has numerous advantages especially in terms of expenditure and compactness. From the obtained experimental outcomes it was noticed that 90.4% and 77% of MO dye was degraded in the coupling and cylindrical reactors respectively.	Peng et al. (2006a), Lee et al. (2001)
Double-side active TiO <sub>2</sub> -modified nanofiltration membranes in continuous flow photocatalytic reactors	Methyl Orange (MO)	By employing UV irradiation on both sides of the membrane, the efficiency of the membrane to photodegrade distinctive water contaminants were assessed. The results indicated that the high water permeability and low adsorption-fouling propensity were observed during the decomposition of methyl orange in the composite NF membranes	Romanos et al. (2012)
Photocatalytic degradation combined with $TiO_2$ membrane assisted on a porous ceramic tube	Acid Red 4	The conclusions of this research work include; (a) three and five times higher decomposition ratios for the dead-end system than the cross-flow system, (b) on enhancing catalyst loading and light intensity, the decomposition ratio has enhanced, but at higher catalyst loading it remained constant (c) and with increasing flow rate the decomposition ratio declined	Wang et al. (2008)

Table 4 Application of nanophotocatalysis coupled with ceramic membrane filtration for the degradation of textile dyes

membranes and their investigations showed that UV irradiation slightly damaged the polymeric membranes.

#### 6 Wastewater treatment using biofilms

Among all biological methods, biofilm technologies play a vital role in the treatment of various wastewaters (Sehar and Naz 2016). Biofilms are composed of several microbial communities bounded in self-generated extracellular polymeric substance (EPS) matrices (Naresh Yadav et al. 2020). The biofilm development has five important phases; (1) The early attachment of planktonic microbes to a solid surface or with one another in an aqueous media; (2) Absolute fixation consequent to the generation of microorganism-moderated EPSs as polyhydroxyl groups and along hydrogen bonding these polyhydroxyl groups seize bacteria to the surface (van Belkum 2007); (3) Development of monolayer mini colonies on the firm surface as attached growth or suspended growth because of the replication of initial colonizers; (4) Biofilm development into 3D form by utilizing the new planktonic bacteria and also by binding the detritus from the adjoining surroundings, and (5) diversification or scattering by passive and active methods in which the matrix-encased biofilm cells

Table 5 Application of biofilm processes for textile dye wastewater treatment

Method	Wastewater	Results	References
Anaerobic biofilm method combined with photo- Fenton oxidation	Textile azo dyes (Remazol Red)	On using the primary Fenton reagent concentration less than 10 mM $H_2O_2$ and 1 mM ferrous ions, COD was diminished to lower than 18 mg/l. Eventually, the toxicity was also reduced by the photo-Fenton oxidation, but the final effluent consisted of high concentrated NaCl. More than 90% of absorbance and COD removal were observed in this study. The obtained experimental outcomes of this research work have recommended the utilization of photo Fenton oxidation after biological treatment for the elimination of toxic and organic pollutants from the textile effluents	Punzi et al. (2015)
Three-stage moving-bed biofilm reactor	Textile dye wastewater	For the biological treatment, polyurethane- activated carbon (PU-AC) (20% v/v) was filled in each reactor and the activated sludge was inoculated into MBBRs. At HRT 44 h, 50% of color and 86% of COD was removed by the MBBR process and this was the significant results for the treatment of dye wastewater	Park et al. (2010)
Dye-degrading bacterial strains such as Lysinibacillus fusiformis strain ZB2, Brevibacillus panacihumi strain ZB1, Bacillus cereus strain ZK2, and Bacillus pumilus strain ZK1	Textile wastewater	The researchers in this study have used sterile sludge as a seeding agent. From the experimental results it was observed that at HRT of 24 h, 46% of COD and 61% of color removal was achieved by the developed granules. The results have revealed that for efficient textile wastewater treatment such as bacterial mixed cultures are highly promising	Kee et al. (2015)

transform into planktonic bacteria through a cell-tocell signaling procedure (Webb 2009; Paridah et al. 2016). Factors that affect the formation of biofilm are nutrients, pH, temperature, the surface topology of support media, velocity, turbulence, hydrodynamics, production of EPS, and divalent cations (Ansari et al. 2017; Krivorot et al. 2011). To allocate the attachment surfaces for biofilm development, the Solid Support Media (SSM) is incorporated in the suspended growth reactors. The addition of SSM enhances the microbial concentration and breakdown the pollutants as well (Pal et al. 2010). The carbonaceous materials, phosphorous, trapped pathogens, nitrogen-containing compounds, and nutrients from the wastewater are degraded by the various microbial populations present in the biofilm matrix. Advantages offered by the biofilm-based wastewater treatment plants are flexibility in operation, less space required, decrease in hydraulic retention time, the less effective over the environment, increase in biomass weight, low sludge production, superior biomass residence time, and superior capability to degrade complex compounds (Martin and Nerenberg 2012; Lewandowski and Boltz 2010). Few recent studies on textile dye wastewater treatment using biofilms are discussed below in Table 5.

Ong et al. (2008) by employing the Granular activated carbon-biofilm configured sequencing batch reactor evaluated the C.I. Acid Orange 7 (AO7) mineralization. The schematic illustration of the granular activated carbon-biofilm configured sequencing batch carbon reactor (SBCR) was shown in Fig. 5. The dimensions of the SBCR was  $20 \times 20 \times 20$  cm and was split into two sections, specifically Multipurpose (MP) and GAC compartments. Granular activated carbon (2.3 1) was used to fill the GAC compartment and using an attachment the azo dye degrading microorganisms were attenuated on GAC. To restraint the DO and to maintain efficacious mixing a mixer was established in the MP compartment. To



Fig. 5 Schematic diagram of granular activated carbon-biofilm configured sequencing batch carbon reactor (SBCR) (Reprinted from (Ong et al. 2008), Copyright (2006) with the permission from Elsevier)

observe the ORP values and the pH, a redox meter and a pH meter were kept in GAC and MP compartments respectively. By submerging the GAC into the anaerobic bioreactor, it was disabled with microbes that degrade the azo dyes. Wastewater containing 2 l of AO7 was fed into SBCR and operated for 24 h cycle time in the ratio of 3:20:0.45:0.15. At 625 mg/L of initial AO7 concentration, less than 0.25 mg/L DO, and in the absence of outside carbon sources, the biological system has achieved almost absolute mineralization of AO7.

### 7 Combination of advanced chemical and biological processes

Major chemical pollutants like pesticides, dyes, solvents, heavy metals, etc. are considered hazardous materials and major threats to the purity of water (Rasalingam et al. 2014). Through wastewater treatment plants or in other ways the chemicals penetrate the aquatic medium and substantial amounts of tenacious substances will be spread over to very long distances from the pollutant's source point. Photodegradation and biodegradation are considered as

the most suitable methods for demolishing the noxious compounds in natural water. Pesticides, phenols, aromatic hydrocarbons, etc. can be degraded by using photodegradation (Van Leeuwen 1996). And in the biodegradation method, generally by using the microbes, the pollutants are eliminated. Studies have revealed that the integration of biological methods with the chemical oxidation processes will enhance the efficiency and lower the operating costs (Oller et al. 2011). Few recent studies on textile dye wastewater treatment using combined advanced chemical and biological processes are discussed below in Table 6.

Rodrigues et al. (2014) worked on the combined Fenton's process and a sequening batch reactor (SBR) for the removal of organic matter and color from polyester, cotton, and acrylic dye wastewaters. To minimize the operating costs and maximize the DOC and color removal, the  $H_2O_2$  and Fe(II) were applied in optimum dosage in the combined process. The installation framework was demonstrated in Fig. 6. At persistent temperature (25 °C) the biological reactor was operated till 10 cycles (12 h/cycle). After adjusting the pH to 7.0 in the first cycle, the biological reactor was supplemented with 2.5 L of wastewater.

Table 6	Application of	f combined	advanced	chemical	and	biological	processes	for	textile	dye	wastewater	treatment
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Method	Wastewater	Results	References
Integrated chemical and biological process	Textile Reactive azo dye	The integrated biological processes ( <i>C. oleophila</i> ) and Fenton's process has decolorized 91% of RB5 dye having an initial concentration of 500 mg/L	Lucas et al. (2007)
Integrated biological biofilm and ozonation	Remazol Black B	The ozonation process acts as the pretreatment for dye degradation. At 500 mg/L of Remazol Black B dye and pH 3–11, about 96% of dye removal was achieved. For the biological treatment, the dye removal has increased with an increase in ozonation time	de Souza et al. (2010)
Combined up-flow biological aerated filter and sequential ozonation process	Brilliant red X-3B azo dye	The ozonation was used as a pretreatment method in which $BOD_5/COD$ has enhanced from 0.1 to 0.4, and in the combined system around 90% of COD removal and 97% of decolorization were achieved	Lu et al. (2009c)
Combined sub-filtration and biological process	Dyeing and printing wastewaters	The wastewater was initially treated by the biological process and followed by a sub-filter method, and 90.9, 92.5, and 91% of average turbidity, color, and CODcr respectively were achieved	Lu et al. (2009b)
Providencia sp. SDS (PS) and Pseudomonas aeuroginosa strain BCH (PA)	Red HE3B	The degradation and decolorization of the Red HE3B by the bacterial consortium (PS & PA) found to be quicker than the independent bacterial strain. Further, during degradation and decolorization process several important dye decolorizing enzymes (DCIP reductase, azoreductase, laccase, veratryl alcohol oxidase) were inducted and it was found that in a 1 h and at 50 mg/L dye concentration 100% decolorization was achieved	Phugare et al. (2011)
Sphingobacterium sp. ATM	Direct Blue GLL (DBGLL)	100% of DBGLL (300 mg/L) dye was decolorized by <i>Sphingobacterium</i> sp. ATM strain in 24 h. Few other textile effluents and mixed dye effluents were also decolorized by the same strain. At the time of DBGLL and other dyes decolorization process, few enzymes (azo reductase, riboflavin reductase, DCIP reductase, laccase, veratryl alcohol oxidase) accountable of degradation were identified	Tamboli et al. (2010)

The final volume was made to 5 L by adding 2.5 L of activated sludge. To reimburse the quantity of treated effluent released, the reactor was supplemented with 2.5 L of effluent. Using air diffusers, the DO content was enabled at  $3 \pm 1.3$  mg O<sub>2</sub>/L and a mechanical stirrer was utilized in the course of reaction stage. The oxidation-reduction potential (ORP), temperature, and pH were frequently observed. Dissolved organic carbon (DOC), COD, BOD5 and TSS were determined at the end of each cycle. Lab view 5.0 software was used to attain automatic unit control and data acquisition. The combined system has shown significant results than individual systems and has shown 99% of color, 91-98% of DOC, 83-95% of BOD, and 88-98% of COD removal. Further, 24-39% of operating costs were reduced by the combined system. In a study, Shah et al. (2012) investigated the enzymatic degradation of Reactive Orange 13 dye using newly isolated bacterial strain *Alcaligenes faecalis PMS-1*. The experimental results have revealed that at static anoxic condition, 24.75 mg/L/h average decolorization was achieved; which is 38.13 times higher than the existing literature results. By using Michaelis– Menten kinetics, the Michaelis constant (K<sub>m</sub>) and the maximum rate (V<sub>max</sub>) were found to be 27.1 mg/L/h and 105 mg/L. At the time of RO 13 decolorization, NADH–DCIP reductase, Tyrosinase, Veratryl Alcohol Oxidase enzymes were noticed.

#### 8 Conclusions

An enormous quantity of water is consumed by the textile industries which release a large amount of



**Fig. 6** Scematic illustration of a Sequencing Batch Reactor (SBR) set-up for textile effluent (Reprinted from (Rodrigues et al. 2014), Copyright (2014) with the permission from Elsevier)

wastewater having organic and inorganic pollutants. To protect the environment from these organic pollutants and to reuse the used water, the effluents are to be treated mandatorily in most places around the world. This short review concludes that various technologies (advanced Physico-chemical and biological) discussed here could be effectively employed in treating textile dye wastewaters. Various wastewater treatment methods are needed to be integrated into the streamlined treatment of contaminated water and also to reach the discharge standard. The techniques considered in the current review are the best befitting options for progressing wastewater at a small scale and also for real industrial wastewater treatment at a large scale. In the present scenario, these treatment methods are stimulating an important level of interest by environmental organizers. Because of potentially longer lifecycles, ease of maintenance, low capital costs, and capability to treat several organic contaminants in wastewater, these methods are considered as expedient. However, only a few studies have discussed treatment costs and the best available technology not entailing excessive cost becomes arduous when there are no-cost figures. Researchers in the coming future should concentrate on cost analysis of the treatment techniques and also on the treatment of complex and single dyes. In this paper, we have critically reviewed and examined the recent developments and progress in the application of photocatalytic materials and biofilms options for advanced textile dye wastewater treatment.

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#### Compliance with ethical standards

**Conflict of interest** The authors declare that there is no conflict of interest.

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